Modeling Solidification Microstructures of Steel Round Billets Obtained by Continuous Casting

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The knowledge of the position of the columnar to equaxial transition (CET) is of paramount importance to evaluate the internal quality of continuous casting (CC) products. One way to control the operational CC conditions with the objective of assuring a given quality level is to develop a numerical program able to calculate the local solidification rate (R), the local thermal gradient (G) and the local time of solidification (t_f) and to relate these parameters to the CET by means of a predictive model. In the present investigation, the dendritic morphology and the CET transition of three round billets made of a low carbon steel (0.14%C) and produced by CC are characterized, and a computer model is developed to evaluate the R, G and t_f-parameters. Referencing the well-known CET transition model developed by Hunt, a simple prediction equation is thus obtained for the steel under study and it is used to propose guidelines for the optimization of the CC operational parameters.

KEY WORDS: continuous casting; columnar to equiaxial ratio; solidification; prediction model; steel round billet.

1. Introduction

The solidification of steel products by continuous casting (CC) is continuously increasing. A fundamental task of the CC method is the optimization of the processing parameters to minimize the formation of defects in the products.[1]

The grain structure of CC products is typically characterized by the presence of small grains in the outer chill zone, elongated grains in the intermediate columnar zone and randomly oriented grains in the central equiaxed zone. The transition from the columnar growth to equiaxed growth (usually called CET) occurs when the columnar front is blocked by the growing equiaxed grains nucleated in the liquid ahead of the solidifying front.[2] The occurrence of such a transition can be predicted by Hunt's model:[3]

$$G < 0.6 \cdot N_0^{1/3} \cdot \Delta T_c \cdot \left(1 - \frac{\Delta T_n^3}{\Delta T_c^3}\right) \quad \text{...............} \quad (1)$$

where G is the thermal gradient at the solidifying front, N_0 is the number density of nuclei of critical size, and ΔT_n and ΔT_c are the nucleation and constitutional undercooling, respectively, in the liquid in which the grains grow.

The position of the CET is an important parameter since it plays a role in the formation of the internal defects. In particular, a large columnar region favors the formation of centerline segregation, cracks and porosity. Several experimental investigations show a clear decrease in the centerline segregation as the equiaxed zone ratio (given by the ratio of the length of the equiaxed to the columnar regions, measured on a product section) increases.[1,4,5] In practice, the equiaxed zone ratio is increased by optimizing the casting parameters such as the casting speed, the superheating of liquid steel in the tundish, and the cooling conditions, or by adopting specific electromagnetic stirrers that break the dendrite tips and thus increase the local density of equiaxed grains.

In steels solidified by CC, solidification occurs with a dendritic morphology in both the columnar and the equiaxed regions. Two parameters are commonly used to characterize such a morphology, i.e., the primary (λ_1) and secondary (λ_2) arm spacing. These parameters can be evaluated by the following relations based on theoretical solidification models:[6,7]

$$\lambda_1 = \frac{N}{R^{1/4} \cdot G^{1/2}} \quad \text{...........................} \quad (2)$$

$$\lambda_2 = M \cdot t_f^{1/3} \quad \text{.................................} \quad (3)$$

where R is the growth velocity of the columnar solidifying front, t_f is the solidification time, and N and M are materials constants.[7] The secondary arm spacing (λ_2) is an important microstructural parameter with regard to internal defects.[5]

To optimize the CC parameters with the aim of reducing the internal defects, it is therefore of paramount importance to develop of a heat transfer model able to predict the parameters G, R and t_f on the product cross section, i.e., at the solidifying front for the whole metallurgical length. In this way it is possible to predict the role of the operating parameters including the tundish superheating, the cooling conditions, and the billet or slab size.

This work investigated the solidification (without stir-

Table 1. Casting parameters.

	Cast speed, m/min	Water flow rate in mould, m³/h	Mould thickness, mm	Temperature increase of cooling water in mould, °C	Cooling water in the secondary region, l/kg-steel
210 mm round billet	1.1	110	18	5.4	0.75
250 mm round billet	1	115	20	5.7	0.55
280 mm round billet	0.8	120	22	5.4	0.45
410 mm round billet	0.5	147	24	5.3	0.3

ring) of CC round billets with different diameters. A computer program was developed to simulate the casting process, and in particular to evaluate the parameters G, R and t_f as a function of the distance from the product surface. A simplified approach is then proposed to estimate the position of the CET and thus to obtain guidelines for the optimization of the CC process.

2. Materials and Experimental Method

Four steel round billets with diameters of 210, 250, 280 and 410 mm were produced by CC. Their nominal chemical composition was: 0.14%C, 1%Mn, 0.3%Si, 0.02%P, 0.015%S, 0.1%Cr, and 0.25%Cu. **Table 1** summarizes the CC operating conditions. The pouring temperature was 1 556°C for each billet, corresponding to a superheat in the tundish of 40°C.

The round billets with a diameters of 210, 250 and 280 mm were submitted to a metallographic investigation. Two sections for each product were investigated with the aim of revealing their dendritic microstructures. For this, the samples were etched with the following solution:[8] 4 g FeCl$_3$, 0.3 g CuCl$_2$, 0.4 ml HCl, 50 ml H$_2$O. The etching duration was in the range of 30 to 60 s. **Figure 1** shows an example of the dendritic morphology in the case of the round with a diameter of 280 mm.

The dendrite arm spacings λ_1 and λ_2 were measured using an image analyzer interfaced with the optical microscope. At the surface of each sample, a magnification of 12.5× was used. At the center, a magnification of 10× was used. The variation of λ_1 and λ_2 as a function of the distance from the surface was then obtained. For each section, the measurements were taken in two positions, *i.e.*, from the surface to the center in two random directions forming an angle of 180°. The reported profiles are therefore the mean values of four measurements.

The microstructural observations also yielded the position of the CET. Four measurements were also taken for this parameter, and the average values are reported.

3. Heat Transfer Model

In CC products solidification starts in the mould where flowing water removes heat through the mould wall. Solidification then continues in the secondary zone, where water sprays remove heat from the solidifying surface. The advancement of the solidifying front up to complete solidification was studied using the Fourier equation for heat conduction under non-steady conditions, with the assumption that heat is extracted in the transverse section along the radial r coordinate (r=0 at the center of the round billet):[1,9]
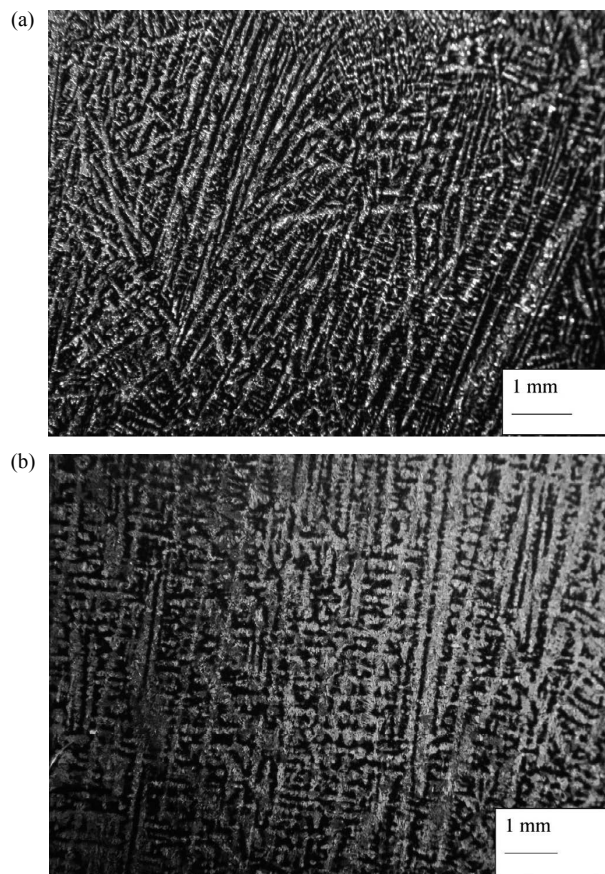
Fig. 1. Example of the dendritic morphology observed close to the surface (a) and at center (b) of the round billet with a diameter of 280 mm.

$$\frac{\delta}{\delta r}\left(k \cdot \frac{\delta T}{\delta r}\right) = \rho \cdot C_p^* \cdot \frac{\delta T}{\delta t} \quad \text{..................... (4)}$$

where T is the temperature, t is time, k is the thermal conductivity of the steel and C_p^*, is its effective specific heat. For solid steel, k depends on temperature, and the relationship reported in Ref. 9 is used. For liquid steel, an effective value was selected to account for the effects of bulk convection. k was set to 100 W/mK, in agreement with data reported in Refs 10 and 11. In the mushy zone, k was calculated using the rule of mixtures. The fraction of solid in the mushy zone, f_s, depends on temperature and on the liquidus and solidus temperatures that were calculated using the relations reported in Ref. 12. The effective specific heat, C_p^*, is defined as:

$$C_p^* = C_p - L \cdot \frac{df_s}{dT} \quad \text{........................... (5)}$$

where C_p is the specific heat capacity of steel (for liquid steel C_p=825 J/kg K, for solid steel C_p depends on temper-

ature,[9] and in the mush zone C_p was evaluated by means of the rule of mixtures), and L is the latent heat of steel (L=272 kJ/kg).

In the mold, the boundary condition was set by considering the following relation for the local heat flux density:[13]

$$q(z) = q_a \cdot e^{-\alpha \cdot z} \quad \text{...........................} \quad (6)$$

where z is the coordinate along the round axis (z=0 at the meniscus), α is a constant (it was set to 1),[14] and q_a is the local apparent heat flux density at the meniscus. It can be determined that:[15]

$$q_a = \frac{\alpha \cdot \Delta T_w^T \cdot \rho_W \cdot C_W \cdot Q}{P_m} \cdot \frac{1}{1 - e^{-\alpha \cdot H_m}} \quad \text{............} \quad (7)$$

where ρ_w and C_w are the density and the specific heat of water at the average temperature in the mold, ΔT_w^T is the total increase in the cooling water temperature, P_m and H_m are the perimeter and length of the mold, respectively, and Q is the volume flow rate of cooling water.

In the secondary cooling region, the boundary conditions are given by the heat exchange due to convection and radiation. The coefficient of convection, h_c, was thus calculated using the following relation:[13]

$$h_c = 392.5 \cdot W_w^{0.55} \cdot \left(1 - 0.0075 \cdot T_w\right) \quad \text{...............} \quad (8)$$

where W_w is the volumetric water flow rate of secondary cooling and T_w is the temperature of the cooling-water spray. The coefficient of radiation was calculated using the usual Stefan-Boltzmann equation. The cooling effect exerted by the rollers played a minor role and was neglected here.

Equation (4) was then solved by the finite-difference method using a program made using Java code. The input parameters of the programme are: steel composition, casting temperature and speed, round billet size, volume flow rate of cooling water in the mold, and the cooling conditions of the different zones in the secondary region.

The program was first validated using the analytical model developed by Alizadeh *et al.*[15] and the shell thickness profile reported in Ming *et al.*[12] In addition, the model was validated by measuring the surface temperatures in different locations on the 410 mm diamater round billet using a pyrometer. **Figure 2** compares the predicted temperature profile with the measured data points, demonstrating that the agreement between the predicted values and the pyrometer measurements is quite good. This procedure could not be
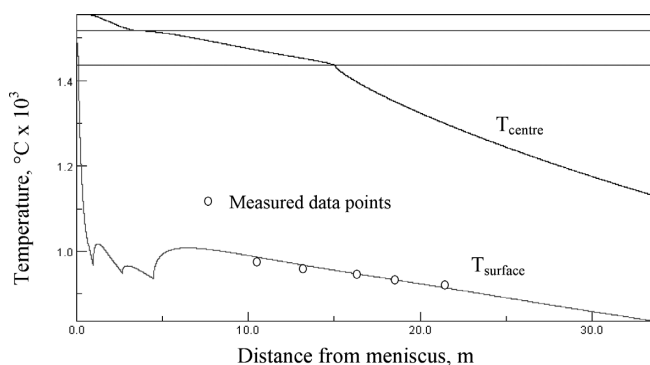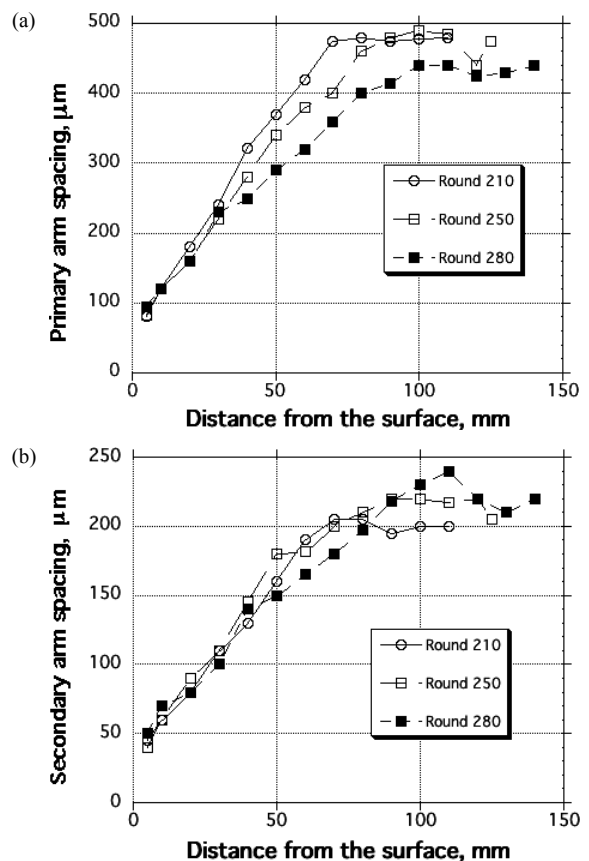
conducted for the other round billets, but we did measure the surface temperatures at the exit of the mold and after the first secondary cooling zone with satisfactory results. For example, the measured temperatures for the 210 mm round billet were 1 180°C and 1 090°C, whereas the predicted values are 1 170°C and 1 085°C. The model is furthr validated indirectly in the next section, where the model predictions are used to estimate the dendrite arm spacings.

4. Results and Discussion

Figures 3(a) and 3(b) presents the results of the metallographic evaluations of λ_1 and λ_2. As expected, and in agreement with the literature data, both λ_1 and λ_2 increase by moving toward the interior of the section, and λ_2 is around one half of λ_1.[7] Further, both λ_1 and λ_2 reach plateaus at the center of the samples, almost at the same distance from the surface. Within the plateau, the scatter of the experimental measurements is higher than in the columnar region (the scatter bars are not reported to avoid undue confusion in the graphs), because λ_1 and λ_2 are more difficult to define there.[8] As already observed,[7,8] this behaviour can be attributed to the transition from columnar to equiaxed growth (CET). This result is in agreement with the experimental measurements of the position of the CET listed in **Table 2** (**Fig. 4** shows a region with the transition from columnar zone to the equiaxed zone). This table also includes the ratios between the CET and the radius of each round billet.

The results shown in Fig. 3(b) further show that the

(a)

(b)

Fig. 3. Average values of primary (a) and secondary (b) arm spacings for the billets under study.

Fig. 2. Comparison between the predicted temperature profile and the measured data points for the 410 mm diamater round billet.

Table 2. Experimental data for the onset of the plateau of λ_2 and for the CET.

	Distance from the surface of the onset of the plateaux of λ_1, mm	CET (experimental measurements), mm	CET/R (radius) ratio
210 mm round billet	70	65	0.62
250 mm round billet	80	77	0.61
280 mm round billet	90	85	0.61
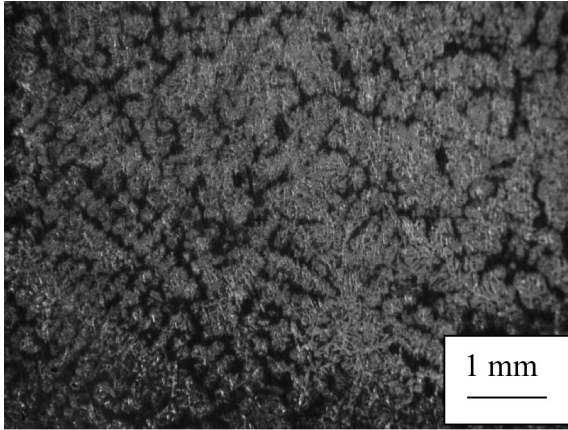
Fig. 4. Region with the transition from the columnar zone to the equiaxed zone, in the 250 mm round billet.

experimental values for λ_2 in the equiaxed zone are quite large, around 220 μm. These values are in agreement with those reported by Choudhary and Ganguly[5] for CC products obtained without electromagnetic stirring.

The heat transfer model can be used to obtain the parameters R, G and t_f as a function of the distance from the surface. To determine R, the solidifying columnar front was set as a fraction of the solid, f_s, of 0.3.[10,11] The following relations were used to G and t_f:[7]

$$G = \frac{\Delta T}{w} \quad \text{...........................} (9)$$

$$t_f = \frac{\Delta T}{R \cdot G} \quad \text{.......................} (10)$$

where w is the length of the mesh ahead of the solidification front and ΔT is the thermal gradient along this length. The results of this evaluation are reported in **Fig. 5**.

According to its definition, R actually represents the velocity of the isotherm for $f_s=0.3$, and it only equals the columnar solidifying front velocity before the CET.[2] The same reasoning is valid for G, and after the CET, G represents the thermal gradient at the isotherm for $f_s=0.3$. As expected, R and G decrease with increasing distance from the surface as long as solidification is columnar. At a certain distance from the surface, R is found to increase rapidly and G to decrease rapidly. A similar effect was also observed by Mapelli and Borgiola[11] and Long et al.[16] A comparison with the data listed in Table 2 shows that this particular behavior is attained in the equiaxed zone. Correspondingly, the solidification time, t_f, is seen to increase with the distance from the surface and to reach a plateau close to the center of the round billet.

As shown by Eqs. (2) and (3), the calculated values of R, G and t_f can be used to evaluate λ_1 and λ_2. For this, the con-
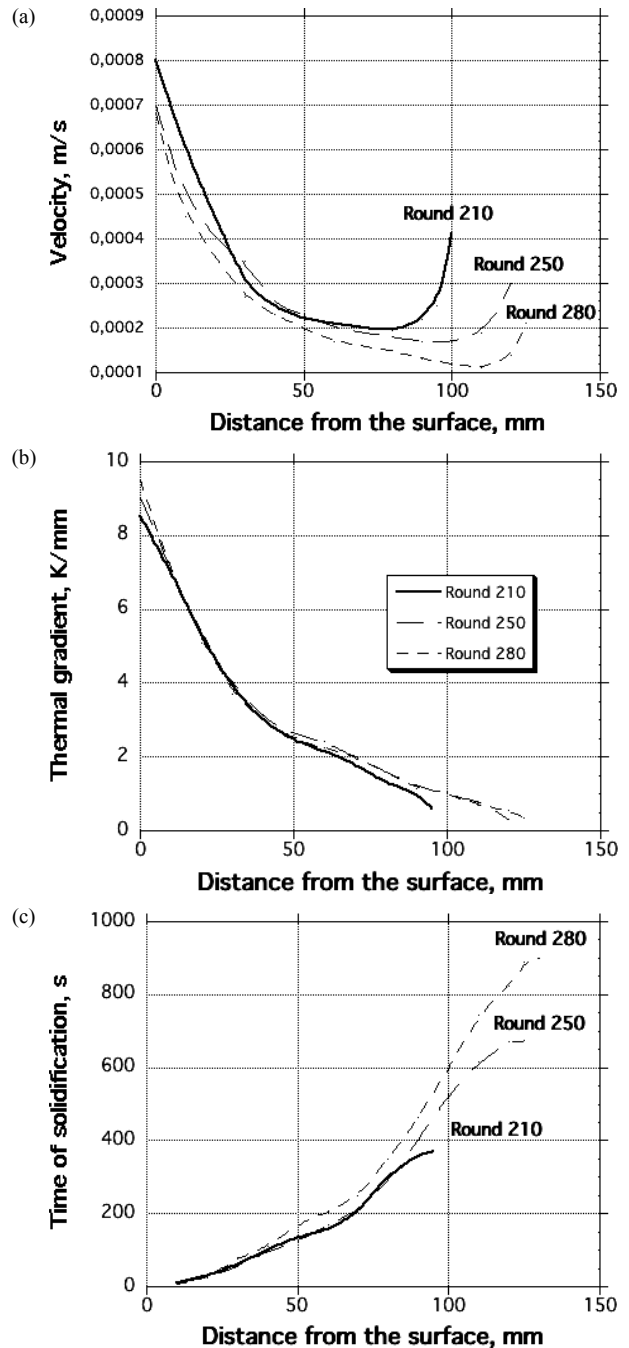
Fig. 5. Calculated solidification parameters: (a) growth velocity of the solidifying front, R; (b) thermal gradient, G; (c) local time of solidification, t_f.

stants N and M can be considered as adjustable parameters. As an example, **Fig. 6** shows the predicted λ_1-values obtained by setting N=70 (with R in m/s, G in K/mm) in the case of the 250 mm diameter round billet. Note that the prediction is very close to the experimental values up to a

distance of about 40 mm from the billet surface, *i.e.*, as long as the solidification growth is columnar. In fact, Eq. (2) is not applicable in the equiaxed region since λ_1 is also influenced by the carbon enrichment of the liquid.[5] The same results have been obtained from the other CC products, and this is a further confirmation of the validity of the thermal model developed here.

From the point of view of the quality of the CC products, the control of the position of the CET is of paramount importance, as stated in the Introduction. In the present investigation, the CET/R ratio is around 0.61 (see Table 2), which is considered as an optimal value for the present production process. However, it is important to understand how changing the operational parameters would influence this ratio.

To determine the influence of the parameters, it is necessary to obtain a procedure able to predict the CET/R ratio as a function of the operational parameters. This can be done according to the approach proposed by Hunt (Eq. (1)). However, this approach is difficult to employ in practice, as it requires the knowledge of several parameters that are not available or can only be computed after the combined thermal and microstructural analysis.[10,11] As shown by Kurz *et al.*,[17] however, the nucleation undercooling can be neglected when R is high (*i.e.*, $\Delta T_n \approx 0$), and the columnar to equiaxed transition occurs when:

$$\frac{G^n}{R} \leq C \quad \text{................................. (11)}$$

where n and C depend on the alloy system.[17] Therefore, from Figs. 5(a) and 5(b), we obtained the values of G and R at the CET, and then we fitted the experimental results using Eq. (11). The obtained values are: n=2.93, C=1.39

10^{13} (with R in m/s, G in K/m). Rapid cooling conditions have been reported when n is between 2 and 3.[17] Equation (11) can therefore be conveniently used to evaluate the role of relatively small variations in the operating conditions from the base conditions.

We first consider the role of casting speed in the case of the 250 mm round billet. Two values of the casting speed were analyzed: 0.9 and 1.1 m/min. From the thermal analysis, the evolutions of G and R were obtained as a function of the distance from the surface, and the dependence of the ratio $G^{2.93}/R$ on this distance was then plotted in **Fig. 7**. The position of the CET was then obtained by observing where such curves intersect the value of C=1.39 10^{13} (with R in m/s, G in K/m). The CET was observed at 72 and 82 mm from the surface of the billet for the 1.1 m/min and 0.9 m/min conditions, respectively.

The obtained data show that the CET decreases as the casting speed is increased, in agreement with data reported in Ref. 10. Of course, as the casting speed is increased, the shell thickness at the exit of the mold is decreased and the metallurgical length is increased, both of which may negatively influence the operational conditions and favor the formation of particular defects such as inner cracks. Table 3 lists the calculated values of all these parameters.

The effect of the tundish superheat was also considered for the 250 mm round billet, using the same approach. Superheats of 30 or 50°C, *i.e.*, 10°C above or below the base value, produced only a weak variation in the CET position, as shown in **Fig. 8**(a). This results is in agreement with published data,[10] and can be explained by considering that a variation in the tundish superheat gives rise to a variation in the evolutions of G and R in such a way that the ratio $G^{2.93}/R$ is not greatly modified. Finally, we considered the

Table 3. Predicted data for the 250 mm round billet.

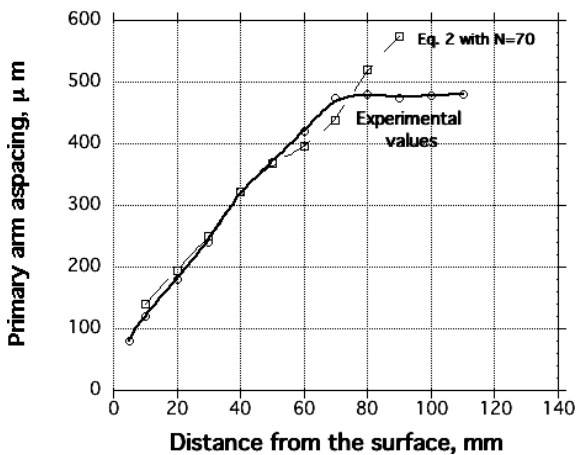| Casting speed, m/min.	Position of the CET, mm	Shell thickness at the mould exit, mm	Metallurgical length, m
0.9	72	14.2	15
1	77	16	16.9
1.1	82	18	18.9

Fig. 6. Experimental and predicted values (by means of Eq. (2)), of the primary arm spacing in the case of the 250 mm round billet.
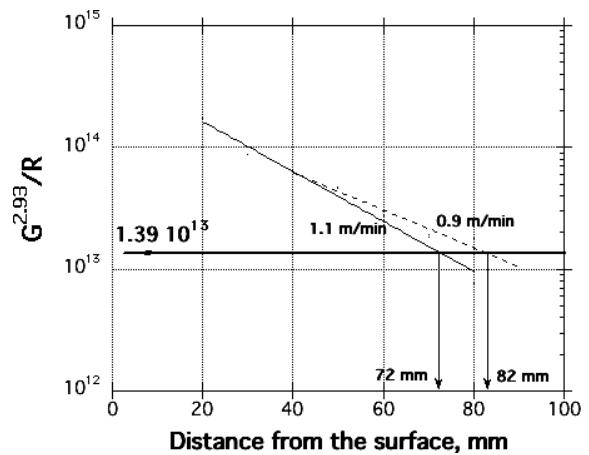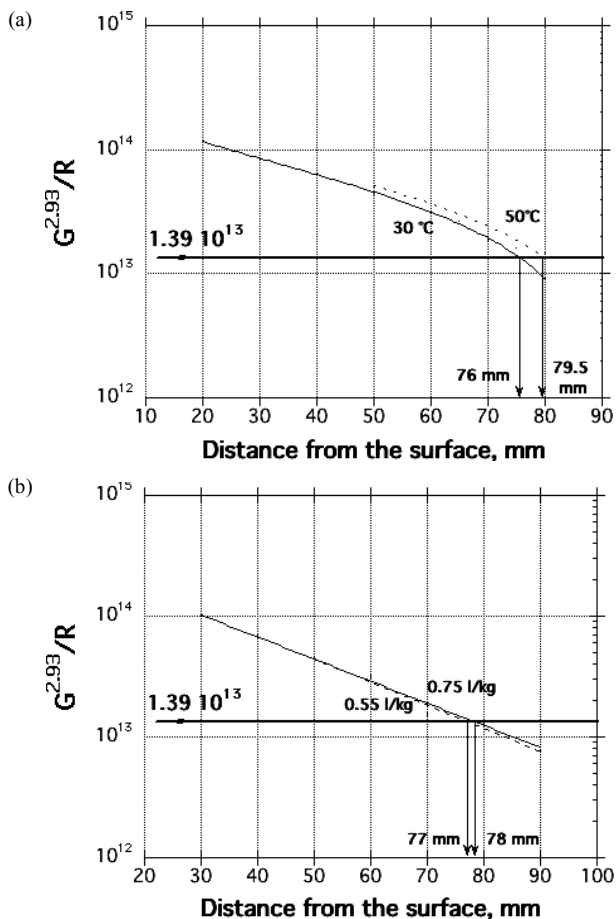

Fig. 7. Estimation of the CET of the 250 mm round billet using Eq. (11) (R in m/s, G in K/m).

(a)

(b)

Fig. 8. Estimation of the CET of the 250 mm round billet using Eq. (11) (R in m/s, G in K/m). (a) role of the superheat; (b) role of the secondary water cooling.

effect of an increase in the intensity of the secondary water cooling to 0.75 l/kg steel (Fig. 8(b)). The position of the CET is predicted to increase to a distance of 78 mm from the billet surface, in agreement with literature data.[10,18]

The analysis presented in this investigation yields several important findings regarding the influence of the operational parameters on the internal quality of CC products. It is quite simple as the parameters n and C of Eq. (11) depend on the steel characteristics and may in principle be obtained from only two experimental datasets. Although the validity of the Hunt's model is widely recognized and the simplification performed to obtain Eq. (11) is fully justified by theoretical and experimental arguments,[10,17] it is clear that this approach requires further confirmation by experimental investigations specific to each situation.

5. Conclusions

(1)   The dendritic microstructures of three round billets made from a low carbon steel (containing 0.14%C) and produced by continuous casting were investigated, and the values of the primary and secondary arm spacing were determined.

(2)   A numerical heat transfer model was then developed and validated with reference to experimental temperature measurements and also with reference to the microstructural characterization. The model was then used to calculate the local solidification time, the local thermal gradient and the local time for solidification as a function of the distance from the round billet surface.

(3)   With reference to the Hunt's model, a simplified relation for the prediction of the columnar to equiaxial transition (CET) was then confirmed and used to relate such a transition to the continuous casting operational parameters. For the steel under study, the transition occurs when:

$$\frac{G^{2.93}}{R} \leq 1.39 \cdot 10^{13}$$

(with R in m/s, G in K/m). In agreement with literature data, the CET was then shown to depend on the casting velocity, the tundish superheat and the intensity of secondary cooling.

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